

SOLVOMET Group

Laboratory of Metallurgical Chemistry







SOLVOMET's vision is that metallurgical chemistry expertise allows to develop more efficient, ecofriendly hydrometallurgical and solvometallurgical processes to provide the critical metals that are needed for the transition to a climate-neutral society.



SOLVOMET's mission is (1) to perform excellent research in metallurgical chemistry and to educate and train young researchers in this domain and (2) to support its Industrial Service Centre partners in the conceptual and practical development of more sustainable (circular, low-energy input) hydrometallurgical (and solvometallurgical) processes, which are subsequently tested using state-of-the-art labscale and mini-pilot-scale experimental facilities.



Background info on Prof. Koen Binnemans & SOLVOMET Group





- Full professor at the Department of Chemistry, specialised in circular hydrometallurgy and solvometallurgy
- Core expertise in critical metals and solvent extraction (SX)
- Author of more than 560 papers, **H-index = 81**, > 29,000 citations
- Former ERC Advanced Grant holder (SOLCRIMET: Solvometallurgy for critical metals)
- **ERC Proof of Concept holder** (SOLVOLi: Solvometallurgy for battery-grade refining of lithium)
- Co-founder SOLVOMET Industrial Service Centre for Hydro/solvometallurgy
- Steercom Member KU Leuven Institute for Sustainable Metals and Minerals (SIM² KU Leuven)
- Former Steercom Member European Rare Earth Competency Network (ERECON)
- Elected member **Royal Flemish Academy of Belgium for Science and the Arts** (KVAB)
- For research domains "hydrometallurgy" & "solvent extraction", according to Google Scholar (data retrieved 2021-07-06), the "world's most cited author".







SOLVOMET's take on the future of hydrometallurgy





Genuine breakthroughs in hydrometallurgy will not come from the use of neoteric solvents like ionic liquids or deep-eutectic solvents, but rather from a deep understanding of hydro-processes at a molecular level. Hydrometallurgy needs to evolve to low-energy-input circular hydrometallurgy.

(Prof. Koen Binnemans, August 2021)



SOLVOMET Group Research Topics

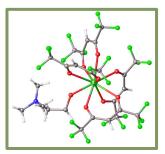


Curiosity-driven fundamental and strategic basic research

- Solvent-assisted metal recovery (SX, direct reduction or hydrolysis in organic phase after SX, antisolvent precipitation, salt crystallisation, SXassisted metal carbonation)
- Circular hydrometallurgy
- Molecular thermodynamics (incl. thermodynamic modelling)

Problem-driven applied and competitive research

- Development of (near-circular, low-energyinput) hydro/solvometallurgical processes (incl. leaching, SX)
- Modelling of hydro/solvometallurgical processes
- Solvent formulation for SX processes
- Validation of leaching and separation processes on mini-pilot scale







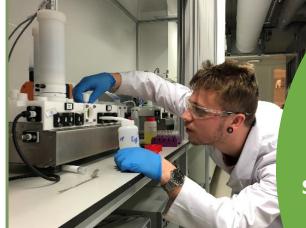




SOLVOMET Group Research domains



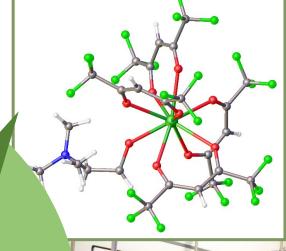




Metal Recovery and Separation Hydrometallurgical and solvometallurgical processes

Circular hydrometallurgy

Predictive thermodynamic modelling







SOLVOMET Industrial Service Centre: Flagship services offered (general overview)



Recovery of metals from ores, solid industrial process residues and urban waste

- ✓ Leaching at lab scale in batch reactors (up to 5 L), mortar grinder or in columns
- ✓ High-pressure leaching in autoclave reactor

2. Removal of metals from liquid (aqueous or organic) process streams

✓ After leaching, metal ions are recovered from pregnant leach solutions by (non-)aqueous SX (see next section), (non-) aqueous ion exchange (IX), cementation or precipitation

3. Solvent extraction processes (SX)

- ✓ SX processes studied from chemical point of view: mechanistic studies and kinetic studies + longterm stability studies of extractants and diluents
- ✓ SX tests in lab-scale mixer-settler batteries, batch extractors, pulsed columns or in series of separatory funnels

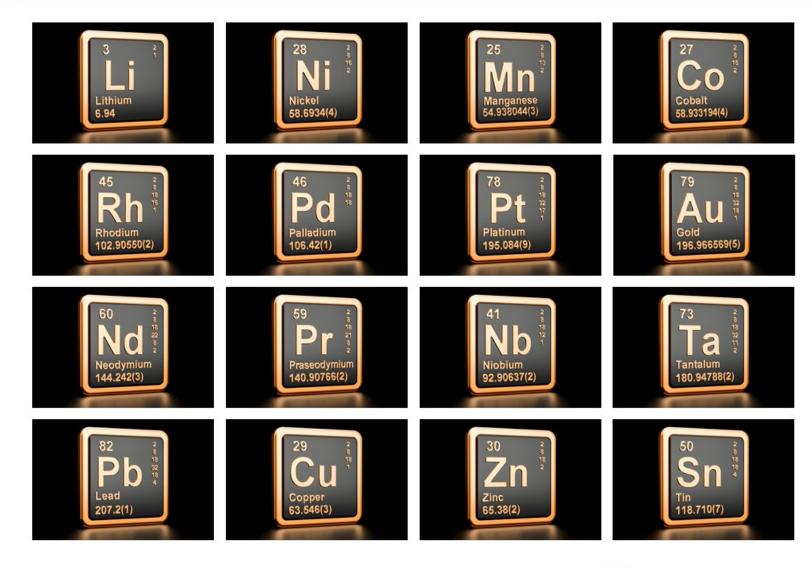
4. Analytical services

✓ QXRD, WDXRF, TXRF, Raman, ICP-OES, ICP-MS, NMR, UV-VIS, SEM-EDS, (EPMA)...



SOLVOMET ISC's key metals of interest







SOLVOMET Industrial Service Centre: Mini-pilot plant facilities for leaching



High pressure reactor

- Effective capacity of 800 mL
- Made from stainless steel with PTFE liner
- Max. pressure = 200 bar
- Max. T = 230 °C with PTFE liner (and 300 °C without)



Multiple reactor system

- 6 reactors (V_{max} = 40 mL)
 with internal stirring
- Individual T & p control
- Max. p = 200 bar
- Max. T = 300 °C, heating rates up to 15 °C/min



Batch leaching reactors

- Two jacketed reactors (1 & 5 L)
- pH and T control
- Digital overhead stirrer
- Filtration system included





SOLVOMET Industrial Service Centre: Mini-pilot facilities for continuous, countercurrent Solvent Extraction (SX) - Mixer-settlers







3 SX mixer-settler set-ups





SOLVOMET Industrial Service Centre: Mini-pilot facilities for continuous, countercurrent Solvent Extraction (SX) - Mixer-settlers Characteristics



Characteristics	SX Kinetics	MEAB	Rousselet Robatel
Temperature	Only room temperature	Only room temperature	Heatable (water or oil)
Operability	Robust, easy to operate. Easy to assemble.	Robust, easy to operate.	Robust. Easy to assemble. The operation requires more attention. Mainly for research.
Visibility	Transparent	Opaque	Opaque but with a window in the settling chamber
Capacity	Mixer: 0.270 L, Settler: 1.050 L	Mixer: 0.12 L, Settler: 0.48 L	Mixer 0.035 L, Settler 0.143 L
Flows (depends on settling velocity)	Max flow: 10 L/h*	Max flow: 10 L/h	Max flow: 2-4 L/h



*the limitation is for the pump, not the mixer-settler

SOLVOMET Industrial Service Centre: Mini-pilot facilities for continuous, countercurrent Solvent Extraction (SX) - Mixer-settlers



	Process	Equipment	Collaboration
PLATIRUS project	Pt, Pd and Rh recovery from spent autocatalysts	MEAB MS	JM Johnson Matthey Inspiring science, enhancing life
Bilateral project with industry	Cu recovery from high-grade Chrysocolla	1 L Hitec Zang leaching reactor and Rousselet MS	© Shell
Fundamental research	Li and Mg separation using binary extractants	Rousselet MS	
	Nd and Dy separation using ionic liquids	MEAB MS	
	Fe, Pb and Zn separation from DES	Rousselet MS	
	Y and Eu separation using non- aqueous solvent extraction	Rousselet MS	







SOLVOMET Industrial Service Centre: Mini-pilot facilities for continuous, countercurrent SX – (Agitated column SX)



Kühni-type agitated column

For processes with low mass transfer, average residence time and high number of stages.

- Jacketed column made from glass with internals made from PEEK
- Max active volume: 0.9 L
- Active height: 1.2 m
- Total Flow: 5-25 L/h (both phases)





SOLVOMET Industrial Service Centre: Lab facilities for lon exchange work (lab-scale column IX set-up)



Econo-chromatography columns

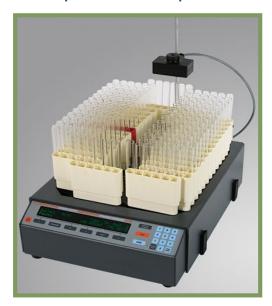
- Low-pressure (<1 bar) or gravity flow separations
- Used in various dimensions (e.g. 0.7 x 30 cm)





CF-2 Fraction collector

- Equipped with drop sensor
- Capacity of 174 tubes
- Coupled with a peristaltic



Ismatec IPC Peristaltic pump

- High-precision 8-channel dispenser
- Flow rates 0.002 44 ml/min





SOLVOMET Industrial Service Centre:

Key analytical facilities & services















SOLVOMET Industrial Service Centre:

Key analytical facilities & services













Publications deriving from bilateral projects with industry – on (solvo)leaching



Journal of Sustainable Metallurgy https://doi.org/10.1007/s40831-020-00294-3

RESEARCH ARTICLE



Ammoniacal Solvoleaching of Copper from High-Grade Chrysocolla

Lukas Gijsemans 10 · Joris Roosen 10 · Sofía Riaño 10 · Peter Tom Jones 20 · Koen Binnemans 10

Received: 22 June 2020 / Accepted: 14 September 2020 © The Author(s) 2020

Abstract

The copper silicate ore chrysocolla forms a large potential copper resource, which has not yet been fully exploited, due to difficulties associated with its beneficiation by flotation and metallurgical processing. Direct acid leaching of chrysocolla causes silica gel formation. Therefore, in this work, the feasibility of solvometallurgical methods to leach copper from high-grade chrysocolla while avoiding issues with silica gel formation was assessed. Ammoniacal solvoleaching was performed with a solvent comprising the chelating extractant LIX 984 N or the acidic extractant Versatic acid 10 in an aliphatic diluent (ShellSol D70 or GTL Fluid G70), combined with a small volume of aqueous ammonia. In the three-phase system, aqueous ammonia dissolves copper from milled and sieved chrysocolla, while copper is simultaneously extracted to the organic phase, releasing ammonia that can be reused for further extraction. The best results were obtained with LIX 984 N as extractant: using a 50 vol% LIX 984 N solution, about 75% of copper could be extracted after 60 min of leaching at 25 °C. The stripping of copper from the pregnant leach solution was optimized. Quantitative stripping of copper was achieved with 1.89 M sulfuric acid and the final aqueous solution of copper sulfate had a concentration of 33 g L⁻¹. Experiments in a leaching reactor (1 L) and small battery of mixer-settlers (3 stages, 35 and 143 mL effective volume in the mixer and the settler, respectively, per stage) were successfully conducted and allowed to recover copper with a purity of 99.9%. A conceptual flow sheet has been developed.

Journal of Sustainable Metallurgy https://doi.org/10.1007/s40831-020-00305-3

RESEARCH ARTICLE



Selective Removal of Zinc from BOF Sludge by Leaching with Mixtures of Ammonia and Ammonium Carbonate

Nerea Rodriguez Rodriguez¹ • Lukas Gijsemans¹ • Jakob Bussé¹ • Joris Roosen¹ • Mehmet Ali Recai Önal¹ • Victoria Masaquer Torres² • Álvaro Manjón Fernández² • Peter Tom Jones³ • Koen Binnemans¹

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Abstract

The zinc content of basic oxygen furnace (BOF) sludges is too high for direct recycling into the blast furnace via the sinter plant, as excessive zinc concentrations are detrimental for the refractory lining of the blast furnace. However, by partial and selective removal of zinc from the BOF sludge, the residual sludge can be used as a secondary iron resource in the blast furnace. In this paper, BOF sludge was leached with aqueous ammonia, aqueous solutions of ammonium salts (chloride, carbonate, and sulfate), and aqueous mixtures of ammonia and ammonium salt. The mixtures of ammonia and ammonium salt could leach more zinc with respect to either the aqueous ammonia or the aqueous ammonium salt solution. The ammonia—ammonium carbonate (AAC) mixture was selected as the most suitable lixiviant due to the high zinc leaching efficiency in combination with a high selectivity towards iron; furthermore, this combination does not introduce unwanted chloride or sulfate impurities in the residue. The leaching process was optimized in terms of the liquid-to-solid ratio, total ammonia concentration, ammonium:ammonia molar ratio, temperature, and leaching time. The co-dissolved iron was precipitated as hydroxide after oxidation of ferrous to ferric ions by an air stream, without co-precipitation of zinc, while the dissolved zinc could be easily recovered as zinc sulfide by precipitation with ammonium sulfide. The (almost) closed-loop process was successfully up-scaled from 10 mL to 1 L scale.

Graphical Abstract

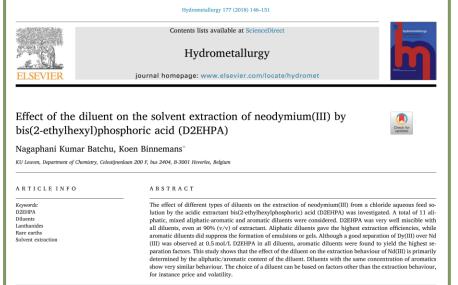




Publications deriving from bilateral projects with industry - on SX









CHEMICAL ENGINEERING RESEARCH AND DESIGN 161 (2020) 304-311

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Selection criteria of diluents of tri-n-butyl phosphate for recovering neodymium(III) from nitrate solutions



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ARTICLE INFO

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ABSTRACT

The selection of a proper diluent should be based on several criteria such as the distribution ratio, phase disengagement time, cost, safety and environmental impact of the process. The effect of different diluents on the solvent extraction of Nd(III) by the neutral extractant trin-butylphosphate (TBP) from nitrate feed solutions was studied. The nature of the diluent had little effect on the extraction kinetics of Nd(III) by TBP above 2.5 min. In general, phase disengagement times were relatively shorter for aromatic diluents compared to aliphatic diluents. Conversely, extraction efficiencies were the highest for aliphatic diluents, slightly lower for mixed aliphatic-aromatic diluents and much lower for aromatic diluents. The poorer extraction efficiencies of aromatic diluents maybe due to the lower concentration of free extractant as a result of the stronger interactions of the diluent with water and/or of the diluent with the extractant. Under the experimental conditions, the differences in extraction between aliphatic and aromatic diluents decreased with increasing the salting-out effect of nitrate ions in the feed. At nitrate concentrations of $4.5\,\mathrm{mol}\,\mathrm{L}^{-1}$ or more, the different diluents had a limited influence on the metal extraction with 1 mol L-1 TBP from feed solutions of 1 g L-1 Nd(III). Thus, under these conditions, the selection of the diluent can be preferably based on its cost, safety and biodegradability rather than on its physico-chemical properties. © 2020 Institution of Chemical Engineers. Published by Elsevier B.V. All rights reserved.



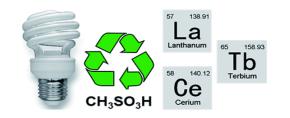
Some key achievements by SOLVOMET



Methanesulfonic acid: a sustainable acidic solvent

Recovery of rare earths from the green lamp phosphor LaPO₄:Ce³⁺,Tb³⁺ (LAP) by dissolution in concentrated methanesulphonic acid







Methanesulfonic acid: a sustainable acidic solvent for recovering metals from the jarosite residue of the zinc industry†



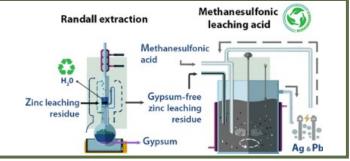




Recovery of Lead and Silver from Zinc Leaching Residue Using Methanesulfonic Acid



From the journal ACS Sustainable Chemistry and Engineering







Broad industrial network



Bilateral projects















Previous collaborations / Active collaborations within H2020 projects







































SOLVOMET's academic network



Some key Projects



















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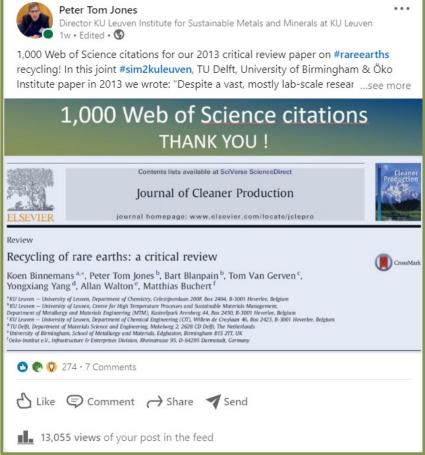




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Scientific & societal impact









COMMENT

Rare-earth recycling needs market intervention

Koen Binnemans n = Paul McGuiness and Peter Tom Jones n |

Nd-Fe-B permanent magnets are essential for the transition to clean energy and mobility. Given the burgeoning demand for neodymium and other rare earths, we discuss the role of recycling and the need for government intervention in securing a sustainable rare-earth supply.

Exactly 200 years ago, in 1821, Michael Faraday demons- If the magnets are required to operate above about 80 °C, trated the first electric motor using a current-carrying then ~1 wt% dysprosium or terbium (both of which are wire, suspended vertically into mercury and rotating much-less-abundant heavy REEs) must be substituted for around a permanent magnet. In January 2021, Norway some of the neodymlum or praseodymlum. The result is reported that two-thirds of car sales at the end of 2020 a family of permanent magnets that offers outstanding were battery electric vehicles (BEVs), meaning they are properties up to about 200 °C, which is sufficient for most the first country in the world where BEV sales outstrip automotive and wind-turbine applications. In the absence those of vehicles powered by fossil fuels. The vital com- of available REEs, we would be forced to substitute ponent in Faraday's laboratory experiment and in the Nd-Fe-B-based motors and generators with alterna-BEVs sold in Norway is the permanent magnet.

about 30 wt% of rare-earth elements (REEs). This group of metals is considered the most critical of raw materials by the European Commission because of its combination of economic importance and serious supply risk. With Since the early 2000s China has supplied more than the prospect of millions of new BEVs, city scooters and electric bicycles on the road and of more electricity gene- has only 37% of the world's total REE reserves, which ration from direct-drive wind turbines, the availability means many REEs could be sourced from other parts of of REEs represents a serious materials concern. In this the world. In South Africa there are plans to restart REE Comment, we look at the status of primary production production at the Steenkampskraal mine, which proand recycling of the key REFs for Nd-Fe-B permanent duced and exported a monazite concentrate during the magnets - neodymium, praseodymium, dysprosium 1950s and 1960s. The company Mkango is exploring and terbium - and discuss whether market intervention for REEs in the Republic of Malawi. The Songwe Hill is required to get REE recycling up and running.

Permanent magnets and substitution

application for which REEs are used but not the only one. Catalysts, batteries, glasses and some metallurgi- extensive REE deposits. In fact, geological analyses cal processes also use large quantities of REEs. Each have shown that Europe has a wide range of primary application tends to demand one or more specific REE, REE resources in Scandinavia and Greenland, which because although REEs are chemically similar, their could easily meet domestic REE demands1. There are, other properties - magnetic, optical, electronic - often of course, barriers, apart from economic ones: environlimit a specific application to a choice of just one or two mental impacts and local protests, in some cases radioof these elements. In some instances, there is the possibility to replace the REE of the REE-containing component with a non-REE alternative, but in many cases there is no realistic option. Let us look at Nd-Fe-B permanent magnets. The basic composition involves about pany Lynas to process REE concentrates from Mount 30 wt% neodymium, which can be substituted, if necessary, by praseodymium (both of which are light REEs).

tives using much weaker magnets like ferrites or alnicos, Faraday's magnet was a lodestone; today's BEVs are which would be bulky and impractical. A dramatic drop powered by neodymium-iron-boron magnets containing in efficiency would be accompanied by a substantial

90% of the world's REE demand. However, China deposit has carbonatite-hosted REE mineralization and has seen previous explorations in the 1980s. The study that is currently ongoing includes a 10,900 m drilling Nd-Fe-B permanent magnets are the largest single programme and has received a £7 million investment Meanwhile, contrary to popular belief, Europe also has today, there is still no operational REE mine in Europe.

> Although Japan does not have any REE deposits or mines, it directly funds the Australian rare-earth com-Weld in a separation plant in Malaysia. In doing so, Japan is trying to secure a sustainable REE supply for

NATURE REVIEWS | MATERIALS

SOLVOMET group

Institute of Metals and

Technology, Ljubljana,

Se-mall- koen binnemansiit

Belalum.

De crux zit in houden wat ie

denken

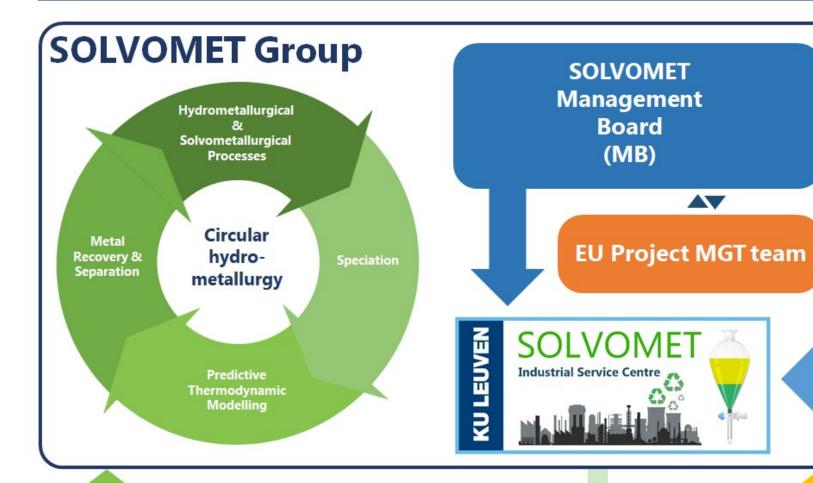
Dat maakt je werkelijk

onafhankelijk'

KU LEUVEN

SOLVOMET Group Governance





Research Team (RT) Junior and senior researchers actively

working in SOLVOMET





Department of Chemistry

or technical and administrative support

SOLVOMET Industrial Service Centre: Project types



Services Agreement (short-term)

- **Project description**: 4-page document describing tasks, deliverables, milestones, budget, timing etc.
- **IP**: foreground IP transferred to company
- **Duration**: typically 6 to 12 months
- **Cost**: salaries of the involved researchers + 50% extra for working budget (chemicals, lab use, travel...)).
- Publications: not planned unless explicitly desired by company in terms of dissemination goals
- Ideal for fast delivery of (confidential) results by experienced (permanent staff) research experts/managers & research associates

Long-term framework agreement

- **Project description**: 4-page document research programme, budget
- IP: foreground IP transferred to company
- Duration: 2 to 5 years
- Cost: salaries of the involved researchers + 50% extra for working budget (chemicals, lab use, travel...)).
- Publications: not planned unless explicitly desired by company in terms of dissemination goals
- Ideal for long-term, in-depth, research support provided by experienced (permanent staff) research experts/managers & research associates

Industrial PhD project

- **Project description**: 4-page document with research programme, budget
- **IP**: foreground IP transferred to company
- Duration: 4 years
- Cost: ~95,000 euro/year [salary + 50% (overhead + working budget for chemicals, lab use, travel...)]
- **Publication clause:** Allowing to publish more generic parts of research while keeping the rest confidential
- Equitable remuneration principle: e.g. preferred partnership for follow-up projects
- Ideal for first-class training of PhD researcher that can go and work for the company later



SOLVOMET is embedded in the KU Leuven Institute for Sustainable Metals and Minerals (SIM² KU Leuven)





Research Line 1

Geological exploration and advanced resource characterisation



Research Line 2

Remanufacturing and demanufacturing



Research Line 3

Sustainable metallurgical processes



Research Line 4

Upcycling processes for primary and secondary resources



Research Line 5

Sustainability assessment and policy research



Research Line 6

Process intensification and digitalisation

simplement problemativen, science-deep research and future-oriented education, contributing to the environmentally friendly production and recycling of metals, minerals and engineered materials, supporting the transition to a climate-friendly, circular-economy.





